Balances on Multiple

Units

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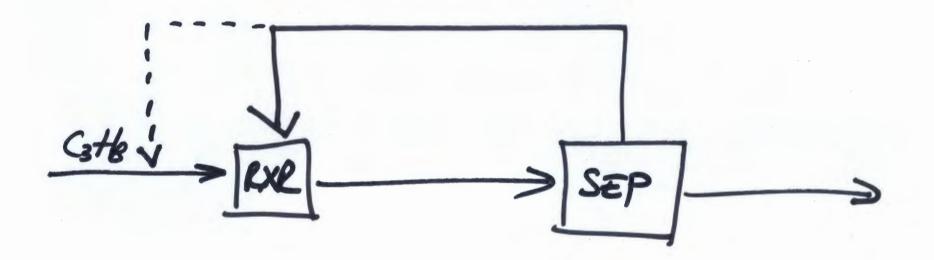
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You Tube: Dr Morrison MTU

Problem: Propane is dehydrogenated to form propylene in a catalytic reactor:

$$C_3H_8 \rightarrow C_3H_6 + H_2$$

The process is to be designed for a 95% overall conversion of propane. The reaction products are separated into two streams: the first, which contains hydrogen gas, propylene (C_3H_6), and 0.555% of the propane that leaves the reactor, is taken off as product; the second stream, which contains the balance of the unreacted propane, 5% of the propylene in the product stream, and no H_2 , is recycled to the reactor. Calculate the flow rates and compositions of all streams and the single-pass conversion of propane in the reactor.



Our first attempt at the flow shut left out the mixing point. We start over.

Reycle - MIX -> RXR) -> SEP -> Rodu Fresh Fud oduct

This is the correct configuration. We now choose a basis + use the ownall conversion. Next: balances on [SEP]



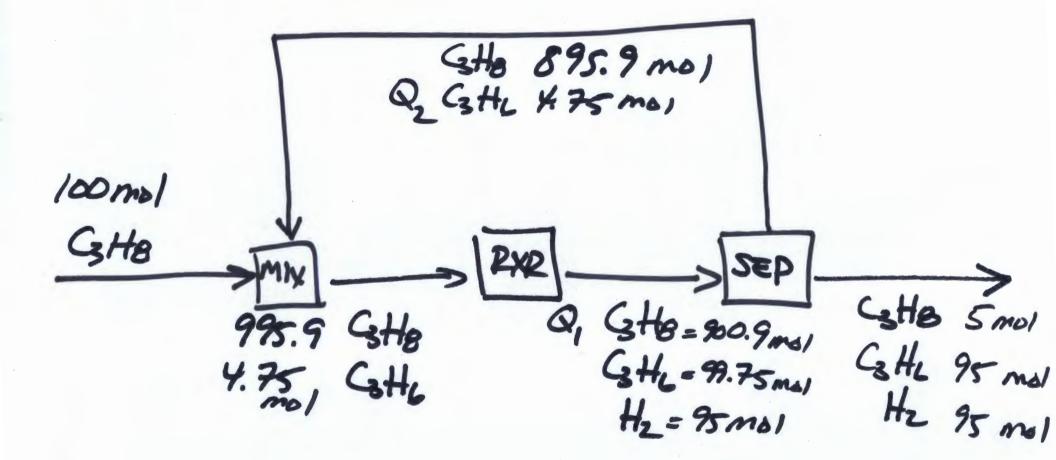
95% conversion

GHO -> GHL+HL

100 mol mass GHB Catle to 3 = 5 moles GHL 5 = 95 moles Hz 3 = 95 mols moles reached 0.95 = moles fed 100 =95 mols overall

BALANES ON SEP Q3 GHB Y.75 may GHL 900.9 mols GHg Smil GH8 99.75 mol Qy GH4 95 may GHL 95 mol Hz 95mol Hz 1) H2 mol BAL 3 GH8 6al 3 GHL MOI BAL $900.9 = Q_3 + 5$ Qy = 4.75 +95 -99.75md Q3= 895.8 md |

USE OTHER Z FACTS:



Smol 0.00555 = Q Q = 900.90 moks

 $Q_2 = 0.05(95)$ $Q_2 = 4.75 mols 1$

Finally, calculate single pass extent of rxn + fractional conversion: RXR. 995.9 mal GH8 (3148=900.9md K.75 mal G.HL GH6=99.75md/ H2=95 mol= 5 f = mous rectice 95 moles fiel = 995.9 = 0.0954