

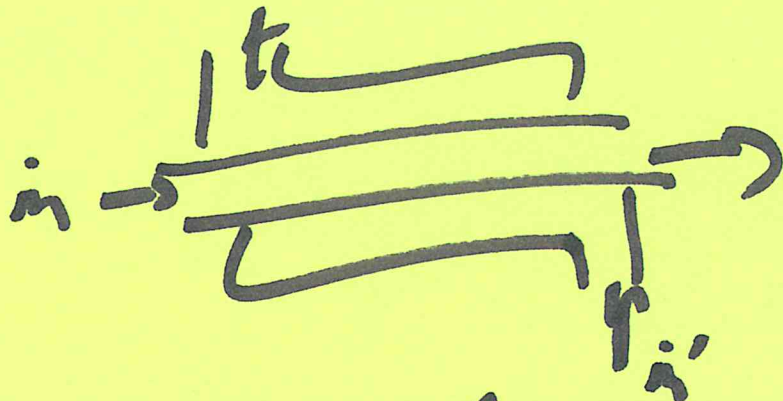
2 DEC 2019
F. Morrison

①

Where were we?

(before Thanksgiving break).....

Applied Heat Transfer



DOUBLE
PIPE

$Q = U A$ (Average driving
"force" for
heat transfer)

$$\Delta T_{lm} = \frac{(\Delta T)_e - (\Delta T)_L}{\ln \frac{(\Delta T)_e}{(\Delta T)_L}}$$

ΔT_{lm}

Shell + Tube HE

②

$$Q = UA \left(F_T \Delta T_{lm} \right)$$

$$F_T = 1 \left\{ \begin{array}{l} \text{double pipe} \\ \text{1-1 shell + tube} \end{array} \right.$$
$$F_T < 1 \left\{ \begin{array}{l} \text{other types} \\ \text{shell + tube} \end{array} \right.$$

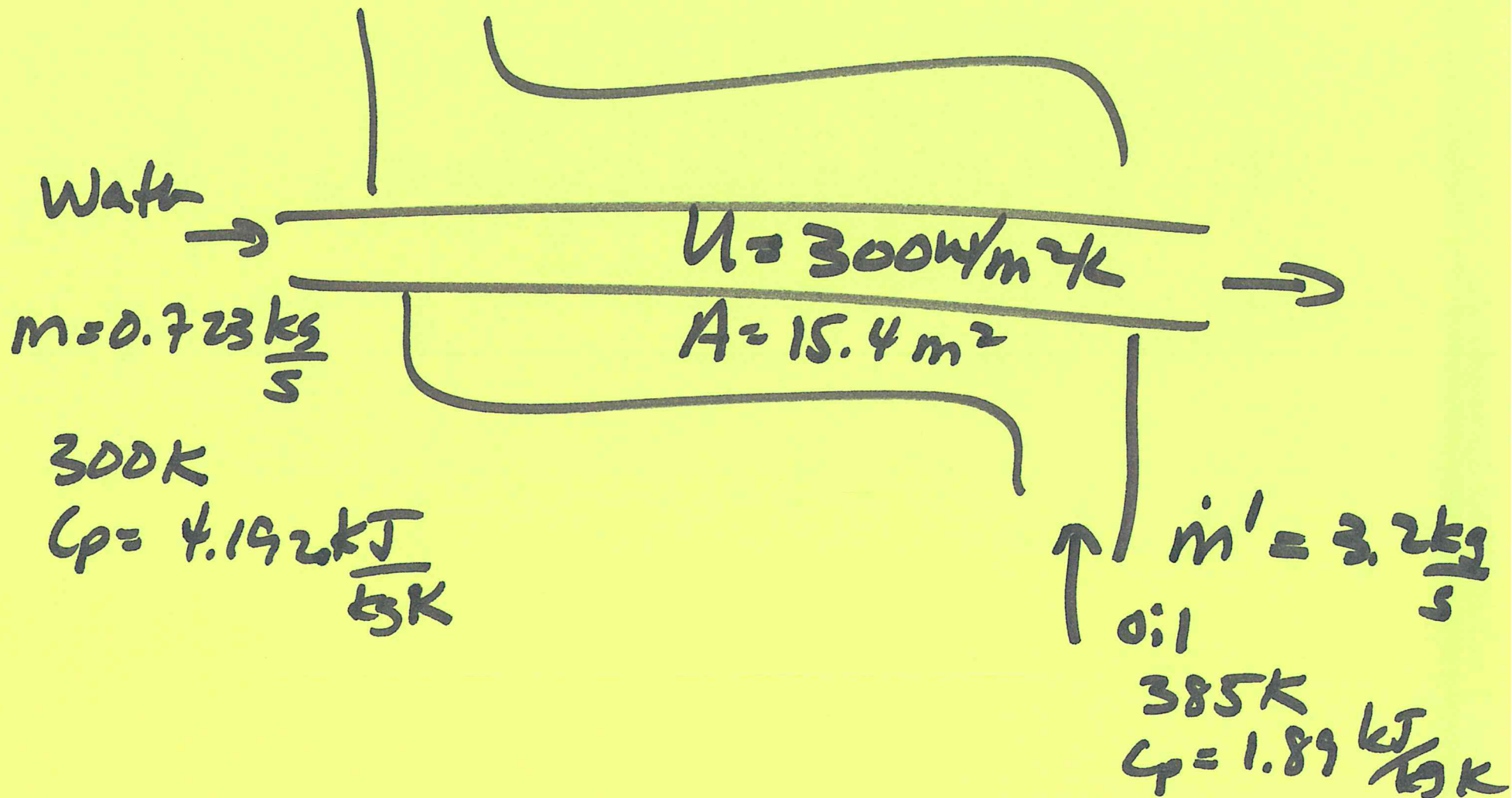
(Usually we do not accept designs w/ $F_T < 0.75$)

HE Effectiveness

Q

EXAMPLE

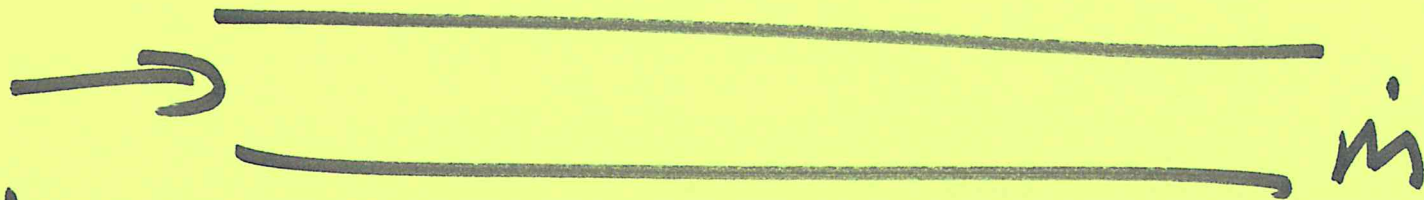
What is Q?



MACRO \bar{E} -BAL INSIDE

②

WATER



$$\dot{m} = 0.723$$

~~$$\Delta \bar{E}_P + \Delta \bar{E}_K + \Delta H = Q_{in} + W_{in}$$~~

$$Q_{in} = \Delta H = \sum_{outs} \dot{m}_i \hat{H}_i - \sum_{ins} \dot{m}_i \hat{H}_i$$

$$-Q'_{in} = Q_{in} = \dot{m} \left(\hat{H}_{out} - \hat{H}_{in} \right) = \dot{m} c_p (T_{out} - T_{in})$$

MASS ENERGY BAL OUTSIDE

(5)

$$\cancel{\Delta E_p} + \cancel{\Delta E_k} + \Delta H = Q_{in} + \cancel{\Delta E_{out}}$$

$$Q_{in}^{(1)} = \Delta H$$

$$= \sum_{out} \dot{m}_i \hat{H}_i - \sum_{in} \dot{m}_i \hat{H}_i$$

$$= \dot{m}' (\hat{H}_{out} - \hat{H}_{in})$$

$$Q_{in}' = \underbrace{\dot{m}'} \underbrace{c_p'} (T_{out}' - T_{in}') \quad \downarrow \quad \downarrow$$

2 EQNS

3 UNKNOWNNS: $Q_{in}, T_{out,w}, T_{out,o,i}$

$$Q_{in} = U A \Delta T_{lm}$$

③

$$\frac{\Delta T_{\text{left}} - \Delta T_{\text{right}}}{\ln \frac{\Delta T_{\text{left}}}{\Delta T_{\text{right}}}}$$

good

3 eqns

3 unknowns

Guess: Q

②

Q	$T_{out,w}$	$T_{out,oil}$	ΔT_{lm}	Q	Match?

OR

⑧

we could use

Heat Exchanger

Effectiveness

...

$$Q = \epsilon (mC_p)_{\min} (T_{hi} - T_{ci})$$

function ϵ : $NTU = \frac{UA}{(mC_p)_{\min}}$
 $\left(\frac{(mC_p)_{\max}}{(mC_p)_{\min}} \right)^{-1}$

EXAMPLE

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① Is it a HE Effectiveness
p/m?

(if Temp in's known
YES)

$$\textcircled{2} (m C_p)_{\text{cold water}} = (0.723) (4.192) = 3.03 \frac{\text{kW}}{\text{K}}$$

$\downarrow C_{\text{min}}$

$$(m C_p)_{\text{hot oil}} = (1.89) (3.2 \frac{\text{kg}}{\text{s}}) = 6.048 \frac{\text{kW}}{\text{K}}$$

$$Q = \sum (mC_p)_{\min} (T_{hi} - T_{ci}) \quad (10)$$

$$\textcircled{3} \quad NTU = \frac{UA}{C_{\min}} = \frac{(300 \frac{\text{W}}{\text{m}^2\text{K}})(15.4 \text{ m}^2)}{3.03 \frac{\text{tCW}}{\text{K}} \left(\frac{10^3 \text{ W}}{\text{tCW}} \right)} = 1.52$$

$$\frac{C_{\min}}{C_{\max}} = \frac{3.03}{6.048} = 0.5$$

$$\epsilon = 0.67$$