

An Introduction to Fluid Mechanics

Faith A. Morrison

Professor of Chemical Engineering

Michigan Technological University

A caution about sign convention

In *Understanding Rheology* (Morrison, 2001) and *An Introduction to Fluid Mechanics* (Morrison, 2012) two different stress sign conventions are used. In the rheology text we follow Bird, Armstrong, and Hassager, *Dynamics of Polymeric Fluids* (Wiley, 1986) ($\underline{\underline{\Pi}} = -\underline{\underline{\tilde{\Pi}}}$, $\underline{\underline{\tau}} = -\underline{\underline{\tilde{\tau}}}$), while in the fluids text we follow the usual engineering sign convention ($\underline{\underline{\tilde{\Pi}}}$, $\underline{\underline{\tilde{\tau}}}$). Any express that contains $\underline{\underline{\Pi}}$ or $\underline{\underline{\tau}}$ is affected.[§]

$$\underline{\underline{\tilde{\Pi}}} = -p\underline{\underline{I}} + \underline{\underline{\tilde{\tau}}}$$

$$\underline{\underline{\Pi}} = p\underline{\underline{I}} + \underline{\underline{\tau}} \quad (\text{Bird et al.})$$

$$\underline{\underline{\tilde{\tau}}} = +\mu(\nabla\underline{\underline{v}} + (\nabla\underline{\underline{v}})^T)$$

$$\underline{\underline{\tau}} = -\mu(\nabla\underline{\underline{v}} + (\nabla\underline{\underline{v}})^T) \quad (\text{Bird et al.})$$

Force on surface with unit normal \hat{n} and area S:

$$\underline{\underline{F}} = \iint_S [\hat{n} \cdot \underline{\underline{\tilde{\Pi}}}]_{surface} dS = \iint_S [\hat{n} \cdot (-\underline{\underline{\Pi}})]_{surface} dS$$

Torque on surface with unit normal \hat{n} and area S:

$$\underline{\underline{T}} = \iint_S \underline{\underline{R}} \times [\hat{n} \cdot \underline{\underline{\tilde{\Pi}}}]_{surface} dS = \iint_S \underline{\underline{R}} \times [\hat{n} \cdot (-\underline{\underline{\Pi}})]_{surface} dS$$

Sorry about that.

Equations for Inside Front Cover

Unit conversions summary: www.chem.mtu.edu/~fmorriso/cm310/convert.pdf

Mechanical Energy Balance	$\frac{\Delta p}{\rho} + \frac{\Delta \langle v \rangle^2}{2\alpha} + g\Delta z + F_{friction} = -\frac{W_{s,by\ fluid}}{m}$	$\begin{cases} \alpha_{laminar} = 0.5 \\ \alpha_{turbulent} \approx 1 \end{cases}$
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$$F_{friction} = \left[4f \frac{L}{D} + \sum_{fittings_i} n_i K_{f,i} \right] \frac{\langle v \rangle^2}{2}$$

**Note error
on inside
front cover:**

Fanning Friction Factor (pipe flow)	$f = \frac{\mathcal{F}_{drag}}{\frac{1}{2}\rho \langle v \rangle^2 \pi R^2} = \frac{\Delta p D}{2L \rho \langle v \rangle^2}$
Drag Coefficient (sphere drop)	$C_D = \frac{\mathcal{F}_{drag}}{\frac{1}{2}\rho v_\infty^2 \pi R^2} = \frac{4gD(\rho_{body} - \rho)}{3\rho v_\infty^2}$

Momentum balance on a CV (Reynolds transport theorem)	$\frac{d\mathbf{P}}{dt} + \iint_{CS} (\hat{n} \cdot \underline{v}) \rho \underline{v} dS = \sum_{\text{on CV}} \underline{f}$
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Hydrostatic pressure	$p_{bottom} = p_{top} + \rho gh$
Hagen-Poiseuille equation (steady, laminar tube flow, incompressible)	$Q = \frac{\pi(p_0 - p_L)R^4}{8\mu L}$

Stokes-Einstein-Sutherland equation (steady, slow flow around a sphere)	$\mathcal{F}_{drag} = 6\pi R\mu v_\infty$
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Macroscopic Momentum Balance on a CV

$$\frac{d\mathbf{P}}{dt} + \sum_{i=1}^{\#streams} \left[\frac{\rho A \cos \theta \langle v \rangle^2}{\beta} \hat{v} \right] \Big|_{A_i} = \sum_{i=1}^{\#streams} [-pA\hat{n}]_{A_i} + \underline{R} + M_{CV} \underline{g} \quad \begin{cases} \beta_{laminar} = 0.75 \\ \beta_{turbulent} \approx 1 \end{cases}$$

Navier-Stokes equation (microscopic momentum balance, incompressible, Newtonian fluids)	$\rho \left(\frac{\partial \underline{v}}{\partial t} + \underline{v} \cdot \nabla \underline{v} \right) = -\nabla p + \mu \nabla^2 \underline{v} + \rho \underline{g}$
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Continuity equation (microscopic mass balance, incompressible fluids)	$\nabla \cdot \underline{v} = 0$
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Total stress tensor $\underline{\tilde{\Pi}} = -p\underline{I} + \underline{\tilde{\tau}}$

$$\begin{pmatrix} \tilde{\Pi}_{11} & \tilde{\Pi}_{12} & \tilde{\Pi}_{13} \\ \tilde{\Pi}_{21} & \tilde{\Pi}_{22} & \tilde{\Pi}_{23} \\ \tilde{\Pi}_{31} & \tilde{\Pi}_{32} & \tilde{\Pi}_{33} \end{pmatrix}_{123} = \begin{pmatrix} \tilde{\tau}_{11} - p & \tilde{\tau}_{12} & \tilde{\tau}_{13} \\ \tilde{\tau}_{21} & \tilde{\tau}_{22} - p & \tilde{\tau}_{23} \\ \tilde{\tau}_{31} & \tilde{\tau}_{32} & \tilde{\tau}_{33} - p \end{pmatrix}_{123}$$

Dynamic pressure $\mathcal{P} \equiv p + \rho gh$

Newtonian constitutive equation $\underline{\tilde{\tau}} = \mu \left(\nabla \underline{v} + (\nabla \underline{v})^T \right)$

$$= \mu \begin{pmatrix} 2\frac{\partial v_1}{\partial x_1} & \frac{\partial v_2}{\partial x_1} + \frac{\partial v_1}{\partial x_2} & \frac{\partial v_3}{\partial x_1} + \frac{\partial v_1}{\partial x_3} \\ \frac{\partial v_2}{\partial x_1} + \frac{\partial v_1}{\partial x_2} & 2\frac{\partial v_2}{\partial x_2} & \frac{\partial v_2}{\partial x_3} + \frac{\partial v_3}{\partial x_2} \\ \frac{\partial v_3}{\partial x_1} + \frac{\partial v_1}{\partial x_3} & \frac{\partial v_2}{\partial x_3} + \frac{\partial v_3}{\partial x_2} & 2\frac{\partial v_3}{\partial x_3} \end{pmatrix}_{123}$$

Total molecular fluid force on a finite surface \mathcal{S} $\underline{\mathcal{F}} = \iint_{\mathcal{S}} \left[\hat{n} \cdot \underline{\tilde{\Pi}} \right]_{\text{at surface}} dS$

Stationary fluid $\left[\hat{n} \cdot \underline{\tilde{\Pi}} \right] = -p\hat{n}$

Moving fluid $\left[\hat{n} \cdot \underline{\tilde{\Pi}} \right] = -p\hat{n} + \hat{n} \cdot \underline{\tilde{\tau}}$

Total fluid torque on a finite surface \mathcal{S} $\underline{\mathcal{T}} = \iint_{\mathcal{S}} \left[\underline{R} \times \left(\hat{n} \cdot \underline{\tilde{\Pi}} \right) \right]_{\text{at surface}} dS$

Total flow rate out through a finite surface \mathcal{S} $Q = \dot{V} = \iint_{\mathcal{S}} \left[\hat{n} \cdot \underline{v} \right]_{\text{at surface}} dS$

Average velocity across a finite surface \mathcal{S} $\langle v \rangle = \frac{Q}{\mathcal{S}}$

Coordinate system	surface differential dS
Cartesian (top, $\hat{n} = \hat{e}_z$)	$dS = dx dy$
Cartesian (side a, $\hat{n} = \hat{e}_y$)	$dS = dx dz$
Cartesian (side b, $\hat{n} = \hat{e}_x$)	$dS = dy dz$
cylindrical (top, $\hat{n} = \hat{e}_z$)	$dS = r dr d\theta$
cylindrical (side, $\hat{n} = \hat{e}_r$)	$dS = R d\theta dz$
spherical, ($\hat{n} = \hat{e}_r$)	$dS = R^2 \sin \theta d\theta d\phi$

Coordinate system	volume differential dV
Cartesian	$dV = dx dy dz$
cylindrical	$dV = r dr d\theta dz$
spherical	$dV = r^2 \sin \theta dr d\theta d\phi$

Coordinate system	coordinates	basis vectors
spherical	$x = r \sin \theta \cos \phi$	$\hat{e}_r = (\sin \theta \cos \phi \hat{e}_x) + (\sin \theta \sin \phi \hat{e}_y) + \cos \theta \hat{e}_z$
	$y = r \sin \theta \sin \phi$	$\hat{e}_\theta = (\cos \theta \cos \phi) \hat{e}_x + (\cos \theta \sin \phi) \hat{e}_y + (-\sin \theta) \hat{e}_z$
	$z = r \cos \theta$	$\hat{e}_\phi = (-\sin \phi) \hat{e}_x + \cos \phi \hat{e}_y$
cylindrical	$x = r \cos \theta$	$\hat{e}_r = \cos \theta \hat{e}_x + \sin \theta \hat{e}_y$
	$y = r \sin \theta$	$\hat{e}_\theta = (-\sin \theta) \hat{e}_x + \cos \theta \hat{e}_y$
	$z = z$	$\hat{e}_z = \hat{e}_z$

$$\text{Divergence Theorem} \quad \iint_S \hat{n} \cdot \underline{F} dS = \iiint_V \nabla \cdot \underline{F} dV$$

$$\text{Stokes Theorem} \quad \oint_C \hat{t} \cdot \underline{F} dl = \iint_S \hat{n} \cdot (\nabla \times \underline{F}) dS$$

Vector identities:

$$\nabla \cdot \nabla \times \underline{F} = 0 \quad (\text{Divergence of curl} = 0)$$

$$\nabla \times \nabla f = 0 \quad (\text{Curl of gradient} = 0)$$

$$\nabla (fg) = f \nabla g + g \nabla f$$

$$\underline{F} \cdot \nabla \underline{F} = \frac{1}{2} \nabla (\underline{F}^2) - \underline{F} \times (\nabla \times \underline{F})$$

$$\nabla \cdot (f \underline{F}) = f \nabla \cdot \underline{F} + \underline{F} \cdot \nabla f$$

$$\nabla \times \nabla \times \underline{F} = \nabla (\nabla \cdot \underline{F}) - \nabla^2 \underline{F}$$

$$\nabla \cdot (\underline{F} \times \underline{G}) = \underline{G} \cdot (\nabla \times \underline{F}) - \underline{F} \cdot (\nabla \times \underline{G})$$