

Macroscopic Energy Balance  
(review from CM2110/CM2120; Felder and Rousseau)

$$\Delta E_k + \Delta E_p + \Delta H = Q_{in} + W_{s,on\ fluid}$$

$$\Delta E_k = \sum_{i,out} \frac{1}{2} m_i v_i^2 - \sum_{i,in} \frac{1}{2} m_i v_i^2$$

$$\Delta E_p = \sum_{i,out} m_i g z_i - \sum_{i,in} m_i g z_i$$

$$\Delta H = \sum_{i,out} m_i \hat{H} - \sum_{i,in} m_i \hat{H}$$

$$= \left[ \sum_{i,out} m_i \hat{U} - \sum_{i,in} m_i \hat{U} \right] + \left[ \sum_{i,out} m_i \frac{P_i}{\rho_i} - \sum_{i,in} m_i \frac{P_i}{\rho_i} \right]$$

note: Geankoplis writes  $-W_{s,by\ fluid}$

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For the following special case (*which is very common in ChE*), we can simplify the energy balance:

- single-input/single output
- small temperature change
- small  $Q_{in}$
- incompressible fluid
- $v$  constant across cross-section

Mechanical Energy Balance

$$\frac{\Delta P}{\rho} + \frac{\Delta(v^2)}{2} + g\Delta z + \underbrace{\left( \Delta \hat{U} - \frac{Q_{in}}{m} \right)}_{\text{friction, F}} = \frac{W_{s,on}}{m}$$

Note:  $\Delta = \text{out-in}$

friction, F

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For systems where the magnitude of  $\underline{v}$  varies across the cross-section:

$$\langle \Delta E_k \rangle = \sum_{i,out} \left\langle \frac{1}{2} m_i v_i^2 \right\rangle - \sum_{i,in} \left\langle \frac{1}{2} m_i v_i^2 \right\rangle$$

Average across the cross-section for the  $i^{\text{th}}$  stream

Recall that the average of a function  $f$  is calculated from:

$$\langle f(x,y) \rangle = \frac{\iint_A f \, dA}{\iint_A dA} = \frac{1}{A} \iint_A f \, dA$$

$$\begin{aligned} \langle \Delta E_k \rangle &= \frac{1}{A_i} \sum_{i,out} \iint \frac{1}{2} m_i v_i^2 \, dA_i - \frac{1}{A_i} \sum_{i,in} \iint \frac{1}{2} m_i v_i^2 \, dA_i \\ &= \frac{1}{A_i} \sum_{i,out} \iint \frac{1}{2} \rho A_i v_i^3 \, dA_i - \frac{1}{A_i} \sum_{i,in} \iint \frac{1}{2} \rho A_i v_i^3 \, dA_i \end{aligned}$$

$m_i = \rho A_i v_i$   
an average mass/length

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$$\langle \Delta E_k \rangle = \frac{1}{A_i} \sum_{i,out} \iint \frac{1}{2} \rho A_i v_i^3 \, dA_i - \frac{1}{A_i} \sum_{i,in} \iint \frac{1}{2} \rho A_i v_i^3 \, dA_i$$

Now we substitute  $\langle v_i^3 \rangle = \frac{1}{A_i} \iint v_i^3 \, dA_i$  and  $m_i = \rho A_i \langle v_i \rangle$

$$\langle \Delta E_k \rangle = \sum_{i,out} \frac{1}{2} m_i \frac{\langle v_i^3 \rangle}{\langle v_i \rangle} - \sum_{i,in} \frac{1}{2} m_i \frac{\langle v_i^3 \rangle}{\langle v_i \rangle}$$

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Following the same logic we used with the macroscopic momentum balance, we define the kinetic energy factor,  $\alpha$

$$\alpha \equiv \frac{\langle v_i \rangle^3}{\langle v_i^3 \rangle}$$

$$\begin{aligned} \langle \Delta E_k \rangle &= \sum_{i,out} \frac{1}{2} m_i \frac{\langle v_i^3 \rangle}{\langle v_i \rangle} - \sum_{i,in} \frac{1}{2} m_i \frac{\langle v_i^3 \rangle}{\langle v_i \rangle} \\ &= \sum_{i,out} \frac{1}{2\alpha} m_i \langle v_i \rangle^2 - \sum_{i,in} \frac{1}{2\alpha} m_i \langle v_i \rangle^2 \end{aligned}$$

$$m_i = \rho A_i \langle v_i \rangle$$

experimental result

$$\begin{aligned} \alpha_{laminar} &= 0.5 \\ \alpha_{turbulent} &= 0.9-0.99 \end{aligned}$$

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Mechanical Energy Balance (with kinetic energy correction)

$$\frac{\Delta P}{\rho} + \frac{\Delta(v^2)}{2\alpha} + g\Delta z + F_{friction} = \frac{W_{s,on}}{m}$$

this is the difference

Note:  $\Delta = \text{out-in}$

**Assumptions:**

- single-input/single output
- small temperature change
- small  $Q_{in}$
- incompressible fluid
- $\alpha$  accounts for non-plug velocity profile

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